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METHOD FOR THERMAL DESIGN OF PADDLE DRYERS:
APPLICATION TO MUNICIPAL SEWAGE SLUDGE

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ABSTRACT

An experimental methodology was developed to improve the energy design of paddle dryers for sewage sludges. A laboratory batch dryer with a vertical agitator has been especially designed and instrumented to determine the heat flux densities. To determine the drying kinetic and the evaporating flow rates, the specific heat and the total heat of desorption of the sludge were measured using calorimetric devices. The evaporating flow rates recorded during the pasty and granular phases were then used in a simple model of the paddle dryer. The good agreement between the computed drying kinetics and the experimental ones measured in an industrial paddle dryer shows that the batch dryer can be used to classify the sludges according to their capacity to be dried in a paddle dryer.

Key Words: contact drying, mixing, drying kinetic, sludge, on site measurement

INTRODUCTION

Sludge management is an ever-increasing problem due to environmental pollution and energy consumption that result from progressive generation of industrial and municipal sludge. For example, the French municipal sludge production was estimated at 850,000 tons of dry matter in 1998, and projected to some 1,300,000 tons in 2005. Drying is now widely recognized as an efficient means of processing municipal sewage sludge to a product that can easily be handled, stored and recycled. After drying, agricultural spreading, landfill and incineration remain available disposal routes. Moreover, the sludge volume is considerably reduced and, due to long residence time at high temperature in most of the conventional dryers, the product is pasteurized.

Thermal drying of industrial sludge has been practiced for many decades but the applications to municipal sludge were rarely reported. In the late 1980s, the manufacturers, who had successfully applied their technologies in chemical and food industries, tried to transfer existing technologies to sewage sludge. Nowadays, few companies possess expertise—successful experience in thermal processing of sewage sludge and, among available technologies, paddle dryers are often encountered in France. Agitation allows to renew the contact surface area between the heated wall and the sludge to keep high heat transfer coefficient. In spite of a great number of industrial applications, the paddle dryer design still remains a question of know how rather than scientific knowledge. The final purpose of our researches is to establish a classification of the sludge according to their capacity to be dried in a paddle dryer but the aim of the present paper is to show that the scaling up methodology is relevant. This methodology lies on sludge characterization, on drying experiments performed at the laboratory scale in a batch agitated reactor, and on drying experiments performed in situ with an industrial Naratherm[®] paddle dryer. Data collected at the laboratory scale are then used in a simple model of the paddle dryer.^[1] The comparison between the drying kinetics determined in the lab scale dryer and the ones measured in situ allows to evaluate the quality of the scale-up protocol.

EXPERIMENTAL APPARATUS

Batch agitated dryer

The experimental set up is fully described in our previous paper.^[2] Therefore, only the main characteristics will be described in the present section. The batch dryer capable of processing up to 5 kg of raw sludge consists of a 0.2m diameter Teflon[®] cylindrical vessel screwed onto the top of metallic plates, which simulate the wall of the dryer ($S=0.0314\text{m}^2$) and its heating system. The stirring device consists of three 0.02 m wide and 0.16 m long blades, sloped at 45° , fixed on a vertical shaft. The distance between the first blade and the dryer wall was set to 0.001 m. Static scrapers are fixed on the Teflon cell to break up the sludge. A motor supplies a constant rotation speed $\omega = 40$ rpm to the stirrer. A torque meter, which monitors the torque during drying, is incorporated into the stirrer drive. The accuracy given by the manufacturer (HBM, Mennecey, France) is ± 0.01 Nm. This setup operates in a closed drying loop to control the temperature, velocity and nature of the gaseous environment. For the present study, flow of superheated steam (1atm, 120°C) was maintained with a velocity less than 0.3 m/s, and the wall temperature was maintained at 180°C . The whole device lays above a scale. During weight measurement, the gaseous flow was bypassed, the stirring device stopped and the cell lowered onto the scale, which has an accuracy of ± 5 g.

Elementary composition analyzer

The elementary composition was measured with a NA 2100 N/Protein analyzer (Thermoquest, Milan, Italy). The measurement accuracy was $\pm 1\%$ for the carbon, hydrogen and nitrogen contents and $\pm 2\%$ for the oxygen content. To estimate the organic fraction of the sludge, 20 grams of dry ground sludge were heated up at 550°C over two hours. Considering that the decomposition of inorganic salts is restricted to

magnesium carbonate at this temperature level and that some of the organic complexes will oxidize only around 700°C, this method gave a rough estimate of the organic fraction. The measurement accuracy was $\pm 0.5\%$.

Calorimeter

The specific heat is an important parameter for sludge processing, not only to calculate the accumulated energy but also for dry sludge temperature control. Indeed, after a drying process and for safety reasons, the dry sludge is often cooled down to ambient temperature in a jacketed screw conveyor. The specific heat of the dry sludge sample was measured using a C80 II calorimeter (Setaram, Caluire, France). A 5g dry sample was heated from 40°C to 100°C at 0.1°C / min. The dry matter specific heat was derived from the calorimetric signal. The measure accuracy has been estimated to 5%.

TGA – DSC apparatus

According to Keey [3], the bonding of condensed moisture to the solid is proportional to the difference between the bound water enthalpy and that of the free water (ΔH_v), at the same temperature and total pressure. This enthalpy difference is called the heat of wetting ($\Delta H_{\text{wetting}}$). The heat of wetting includes the heat of sorption, hydration and solution and is a function of the moisture content.

Reports on direct measurements of the heat of wetting are scarce ([4], [5]). For a well characterized solid adsorbent, like zeolite or graphite, the value can be theoretically calculated [6] but in the case of complex heterogeneous solids, like foodstuff or sludge, the value is generally derived from water activity data using the Clausius-Clapeyron law ([7], [8]).

A thermogravimetric analyzer (TGA) coupled with a differential scanning calorimeter DSC111 (Setaram, Caluire, France) used in isothermal mode enables a direct and continuous measurement of the total heat of sorption as a function of the moisture content. The total heat of sorption is derived from the calorimetric signal and the mass loss [9].

LAB SCALE DATA PROCESSING

The drying kinetics were computed from an energy balance rather than determined from the mass measurements, which are discontinuous. The data processing and the assumptions made are described in the sections that follow.

Energy balance

As weighting measurement is discontinuous and a lot the drying experiments is disturbed, the evaporating flow rate \dot{m} is calculated from an energy balance on the product, written as follow:

$$\frac{\partial}{\partial t} (m_s C_{p_s} T_s) = \phi S + h_{s-v} S_{free} (T_v - T_s) + 2\pi C_{eff} \frac{\omega}{60} - \dot{m} (\Delta H_v + \Delta H_{wetting}) \quad (1)$$

where the first term corresponds to the energy accumulated in the sludge, ϕ is the heat flux density supplied by conduction at the heated wall of the dryer, h_{s-v} is the heat transfer coefficient between the free surface of the product in the vessel, S_{free} , and the gas, C_{eff} is the effective mechanical torque, ΔH_v is the latent heat of vaporization, and $\Delta H_{wetting}$ is the heat of wetting.

The specific heat of the wet sludge, C_{p_s} , is a function of the moisture content and the temperature. If the moisture content is known, it can be computed from the specific heat of the water, C_{p_w} , and that of the dry sludge, $C_{p_{DM}}$, according to equation (2):

$$C_{p_s}(W, T) = \frac{W}{1+W} C_{p_w}(T) + \frac{1}{1+W} C_{p_{DM}}(T) \quad (2)$$

$C_{p_{DM}}$ is measured with the C80II Calorimeter and the experimental data can be adjusted with a linear expression, as follows:

$$C_{p_{DM}} = \beta T + \delta \quad (3)$$

where β and δ are two constants.

Once \dot{m} is known, the drying kinetics are computed from equation (4):

$$W(t) = W_{\text{initial}} - \frac{1}{m_{\text{DM}}} \int_0^t \dot{m} dt \quad (4)$$

where m_{DM} is the dry mass.

During the experiment, the product and vapor temperatures as well as the effective mechanical torque are continuously recorded while the rotation speed is known. To compute the evaporating flow rate from equation (1), it was also necessary to evaluate the heat flux density supplied by the dryer wall, ϕ , the heat transfer coefficient between the product and the vapor, h_{s-v} , and finally the free surface of the product, S_{free} .

Dryer wall heat flux density estimation

The dryer wall and its heating system, reproduced schematically in figure 1, consists of:

- a heating device made of ten electrical resistors inserted in metallic plates. Each resistor can supply up to 250W;
- a 0.01 m thick buffer copper plate for temperature homogenization. A temperature sensor, set at 0.001 m from the buffer copper plate front side, is used for thermal regulation;
- a 0.01 m thick stainless steel plate, which simulates the wall of the dryer. Four sensors, set at 0.0015 m from the steel plate front side, measure the temperature at different radii (0.015, 0.055, 0.075 and 0.095 m) from the center and one sensor, set at 0.001 m from the steel plate rear side, measure the temperature at a radius of 0.035 m from the center.

The accuracy of all these thermal sensors with their acquisition lines was evaluated at $\pm 0.15^\circ\text{C}$.

The heat flux density ϕ exchanged between the stainless steel plate and the product could be estimated either from the electrical power or from the temperature measurements. In the first case, ϕ is given by the difference between the electrical power P supplied by the resistances, which is measured during the drying experiment, and the heat losses P_{lost} , estimated from experiments performed with an empty setup in the same operating conditions.

$$\varphi = \frac{1}{S} (P - P_{\text{lost}}) \quad (5)$$

The parameter φ can also be estimated by solving the inverse conduction problem in the dryer wall. The numerical method is extensively described in Fudym et al. [10]. Because of the buffer copper plate, the rear side temperature of the stainless steel plate is assumed to be homogeneous. On the front side, radial temperature gradients are quite high due to stirring of the drying material. To take them into account, an influence area was assigned to each thermocouple set on the front side of the steel plate. This area was defined by:

$$S_i = \pi \left((r_i + l_{iR})^2 - (r_i - l_{iL})^2 \right) \quad (6)$$

where S_i is the influence area assigned to the thermocouple located at the radius r_i , l_{iR} and l_{iL} are the distances, reported in Table 1, between the edges of the ring area and the position of the thermocouple.

The one-dimensional conduction problem is solved in each concentric zone and the heat flux density φ at the dryer wall is computed from the heat flux densities φ_i estimated in each zone S_i according to:

$$\varphi = \frac{1}{S} \sum_{i=1}^4 \varphi_i S_i \quad (7)$$

where $S = \sum_i^4 S_i$.

Heat transfer coefficient and free surface estimations

Three distinct phases occur during drying [2]. Transitions from the fluid state to the sticky one and finally to the granular phase, which are evident from the heat flux signal, are better seen the torque evolution curve (cf. Figure 2). Over first few minutes, the sludge behaves like a viscous fluid and the contact with the heated wall is rather good. During this first stage, the free surface of the product is almost equal to the heated surface ($S_{\text{free}} = 0.0314 \text{ m}^2$) and the heat transfer coefficient h_{s-v} between the free surface S_{free} of the product and the vapor results from the vapor flow above the product. The magnitude of h_{s-v} was estimated at $7 \text{ Wm}^{-2}\text{K}^{-1}$ from experiments performed with the setup empty, computing the

heat flux density supplied by conduction with the inverse method and recording the wall and vapor temperatures.

As drying continues, the sludge becomes sticky, accumulates in dead volumes or sticks on the stirring device. Due to the dryer geometry, the contact with the heated wall is reduced and, as a consequence, the heat flux density supplied to the product by the heated plate is very small. Nevertheless, weight measurements show that the mass loss is significant. Thus, during this second phase, the product is mainly dried by convection and conduction through the stirring device. As it was not possible to assess neither the heat transfer coefficient h_{s-v} nor the free surface S_{free} , the measured and calculated mass loss values were adjusted and the product $h_{s-v} * S_{free}$ estimated at 6.4 WK^{-1} .

At the end of the sticky phase, the granular phase appears and the heated surface is again fully covered by the product and the geometric configuration is similar to the one observed during the fluid phase. Thus the previously estimated values for the heat transfer coefficient h_{s-v} and the free surface S_{free} can be used in a first attempt.

VALIDATION OF THE DATA PROCESSING

Drying experiments were performed with a digested sewage sludge, named A in the following sections. Its characteristics are reported in Table 2. The values of the two constants, β and δ , used to adjust the dry matter specific heat (eq. 3) as well as the correlation coefficient are given in Table 3. The heat of wetting, plotted in Figure 3, can be neglected as long as the moisture content remains higher than 0.3 kg/kg DM . However, when the moisture content further decreases, the heat of wetting strongly increases and, for instance, reaches a value between $1\ 500$ and $2\ 500 \text{ kJ/kg}$ for a 0.05 kg/kg DM moisture content. These orders of magnitude are in agreement with those reported by Herwijn [11] but are lower than those achieved by Chen et al. [12]. According to Laidler and Meiser [13], this corresponds to an intermediary step between the physical adsorption and chemisorption/chemical reaction.

For the drying experiment, the operating conditions were fixed to 180°C for temperature of the heated surface and 3.5 kg for the initial mass of the sludge. The estimated heat flux densities, computed from temperature measurements and from the electrical power, are plotted in Figure 4 versus drying time. The agreement between the two methods is rather good except for the transition towards the granular phase when the plate is suddenly coated with the wet granular matter. According to these results, the estimation of the heat flux is considered correct and either of the two methods can be used for the determination of the heat flux density supplied to the product by conduction.

Weight measurements were performed during this drying experiment. The calculated and measured drying kinetics are compared in Figure 5. The good match of the computed values and the measured ones validates the data processing. Since computation offers accurate predictions, it was decided to use the energy balance for the determination of the drying kinetics in all experiments.

DRYING RATE CURVE AT THE LAB SCALE

According to the recommendations made by Kemp et al. [14], the moisture content - time data were smoothed using a cubic spline fit over a number n of adjacent data points and the drying rate – moisture curve (derivative of the previous curve) calculated from the spline equation. The first part of the moisture content – time curve, corresponding to the initial heating of the product, and the following part were adjusted separately. As smoothing tends to conceal information, the fit sensibility to the number n of adjacent data points was investigated by comparing the drying rate curve obtained by differentiation of the experimental data with the smoothed curve. It was found that $n= 270$ gives the most sensible data fitting. With this processing method, the difference between the raw moisture contents and the smoothed data is always less than 4%.

The drying rate – moisture curve, plotted in Figure 6, exhibits three different stages previously described. So as not to overload this figure, the moisture contents corresponding to the transitions toward

the lumpy and granular phases are given in Table 4 as well as the mean evaporating flow rates per heated surface area computed for each phase. Since the free surface of the product was to a great extent unknown, it was not possible to plot the classical drying rate curve $N = f(W)$. However, a more or less constant rate period was observed during the pasty phase ($W \geq 3.6$ kg/kg DM). In the same time, the sludge temperature remained equal to 100°C (cf. Figure 3). The decrease of the evaporating flow rate, observed for $3.2 \leq W \leq 3.6$ kg/kg DM, is attributed to a reduction of the contact surface between the sludge and the heated wall. Between 3.0 and 0.32 kg water/kg dry matter, the sludge becomes sticky and, as a consequence of the vertical design of the lab scale dryer in which the sludge is not compressed against the heated wall, the contact between the sludge and the heated wall is imperfect and the drying rate low. At the end of this sticky phase, the granular phase appears. Moist sludge is again in contact of with the heated wall. A linear decrease of the evaporating flow rate is recorded during this period.

FROM THE LABORATORY SET UP TO THE INDUSTRIAL PADDLE DRYER

Wastewater treatment plant description

The in situ drying experiments were performed in a biological wastewater treatment plant, which was equipped with a Naratherm[®] paddle dryer. This plant treats industrial wastewater (85%) and municipal wastewater (15%). The annual sludge production is around 400 tons of dry matter. Before drying, the sewage sludge (named sludge B in the following) is thickened by dissolved-air flotation, conditioned and dewatered by centrifugation. The Naratherm[®] paddle dryer consists of a 3.6 m long horizontal jacketed trough with two 22 rpm rotating shafts. On each shaft, hollow wedge-shaped paddles are welded. To ensure good mixing in any point of the dryer and plug flow along the trough, the paddles penetrate along the shafts. The sludge is fed into one end and moves along the trough owing to gravity and rotation of the paddles. The dry material is discharged at the opposite end. All metallic surfaces in contact with the sludge (the jacket, the hollow shafts and paddles) are heated with saturated steam at a pressure close to 6

bar. This 32 m^2 heated surface area is self-cleaned because of friction forces induced by rotors motion. Vapors evolved during processing are carried out through a central exhaust port.

In theory, these indirect dryers [15] can treat the sludge in a single stage without back mixing but in practice the production of small dry pellets is significant (due to an over designed mechanical stirring) and a huge amount of dry product is recirculated in the dryer. As the production of small dry pellets was significant, 45% of the dry product was recirculated in the dryer. Thus, the feeding flow rate was equal to 267 kg of dry solid per hour and the inlet moisture content of the sludge 1.5 kg water/kg dry matter. The residence time of the sludge in the dryer was estimated to five and a half hours. At the dryer inlet, the sludge has a pasty consistency. As its moisture content decreases, the sludge becomes sticky and breaks into pellets. The transition between the pasty phase to the granular one appears at a distance of $z_{\text{transition}}=1.43 \text{ m}$ from the dryer inlet, this corresponds to $0.35 * L$, L being of the dryer length (L). The outlet moisture content of the sludge is around 0.07 kg water / kg dry matter. This general behavior has already been reported by Yamahata and Izawa [16]. According to their comments, the length of the paste zone ranges between 0.26L and 0.33L.

Simple paddle dryer model

According to our observations in situ and at the lab scale, a simple paddle model has been proposed [1]. The following assumptions were made:

- ✓ The dryer is divided into a paste zone and a granular one;
- ✓ The paste zone ranges between the dryer inlet and $z_{\text{transition}}$ and the evaporating flow rate per unit surface of the dryer is assumed to be constant and equal to the value recorded at the lab scale;
- ✓ In the granular zone, the product height in the dryer is equal to the paddle diameter and, thus, the contact surface is reduced to the sum of the two mixer shafts surface, the shaft mounted paddles

surface and a small part of the jacketed trough surface. A linear decrease of the evaporating flow rate per heated surface of the dryer with the moisture content is assumed;

- ✓ Finally, a plug flow and a homogeneous moisture distribution in each cross section of the dryer are assumed.

The following mass balance can be written on a small control volume:

$$\dot{m}_{DM} \frac{dW}{dz} = -F \frac{A}{L} \quad (8)$$

where \dot{m}_{DM} and $A dz/L$ are the dry mass flow rate and the elementary heated surface, respectively. The evaporating flow rate per heated surface F depends on the physical state of the sludge in the dryer:

$$\begin{aligned} F &= \text{const} \quad \text{for} \quad W_{\text{granular}} \leq W \\ F &= a * W + b \quad \text{for} \quad 0.05 \leq W \leq W_{\text{granular}} \end{aligned} \quad (9)$$

which yields:

$$W(z) = W(z=0) - \frac{F}{\dot{m}_{DM}} \frac{A}{L} z \quad \text{for } z \leq z_{\text{transition}} \quad (10)$$

$$W(z) = W(z_{\text{transition}}) \exp\left(-\frac{a}{\dot{m}_{DM}} \frac{A}{L} (z - z_{\text{transition}})\right) \quad \text{for } z_{\text{transition}} < z \quad (11)$$

When the evaporation flowrates in the pasty and granular phase are known, the moisture content distribution along the dryer can be computed.

Validation of the paddle dryer model

Sludge B was characterized at the lab scale (Arlabosse et Chavez, 2004). The main characteristics of sludge B are reported in Table 2. The elementary analysis leads to a chemical formula closed to the cellulose one $(C_6H_{12}O_5)_n$. The evaporation flow rates were determined from the drying experiment performed in the batch agitated dryer at the lab scale. The moisture contents corresponding to the

transitions toward the lumpy and granular phases, the mean evaporating flow rates are reported in Table 4. From the drying kinetics, the two constants a and b were estimated at 34.38 kg dry matter/m² h and 4.58 kg water/m² h, respectively. Using equations (10) and (11), the drying kinetics in the paddle dryer are computed and compared to the ones measured experimentally. As can be seen in Figure 7, the agreement between computed and measured kinetics is rather good. This confirms the assumptions made, specially that of a plug flow in the dryer.

CONCLUSIONS AND FURTHER DEVELOPMENTS

Since the thermal design of the paddle dryer is empirical, a methodology has been developed to investigate the drying kinetics of the sludge in this type of a dryer. At the lab scale, drying experiments are performed in a batch agitated vertical dryer. The drying kinetics and the evaporation flow rates are computed from an energy balance, which requires the knowledge of the specific heat and the total heat of desorption besides the temperature measurements. These kinetics exhibit three different zones, depending on the consistency of the sludge. A constant evaporation flow rate is recorded in the pasty phase whereas a linearly decrease is observed during the granular period. Besides these experiments at the lab scale, a simple model of the paddle dryer has been proposed. The main assumption of this model concerns the division of the dryer in pasty and granular zones. Data collected at the lab scale are used to compute the moisture content distribution along the dryer. Good agreement between the calculated distribution with that measured in situ on the industrial Naratherm[®] paddle dryer shows that measurements obtained at the laboratory scale are sufficiently representative. Future experimental investigations will focus on the influence of the sludge origin and treatment on the drying kinetics and the thermal design of the paddle dryer. The final goal is to establish a classification of the sludge according to their capacity to be dried in a paddle dryer.

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NOMENCLATURE

| | | |
|----------------|--|--|
| A | Heated surface of the paddle dryer | (m ²) |
| a | Constant used in equation (9) | (kg DM.m ⁻² .h ⁻¹) |
| b | Constant used in equation (9) | (kg water.m ⁻² .h ⁻¹) |
| C | Mechanical torque | (N.m) |
| C _p | Specific heat | (J.kg ⁻¹ .K ⁻¹) |
| F | Evaporating flow rate per heated surface | (kg.m ⁻² .s ⁻¹) |
| h | Heat transfer coefficient | (W.m ⁻² .K ⁻¹) |
| L | Dryer length | (m) |
| l | Distance between the edges of the ring area and the position of the front thermocouple | (m) |
| m | mass | (kg) |
| \dot{m} | Evaporating flow rate | (kg.s ⁻¹) |
| P | Electrical power | (W) |
| S | Heated surface | (m ²) |
| r | Radius | (m) |
| T | Temperature | (°C) |
| W | Moisture content dry basis | (kg water.kg ⁻¹ dry solid) |
| z | Abscissa | (m) |

Greek letters

| | | |
|----------------------|-------------------------------|--|
| β | Constant used in equation (3) | (J.kg ⁻¹ .K ⁻²) |
| δ | Constant used in equation (3) | (J.kg ⁻¹ .K ⁻¹) |
| ΔH_v | Latent heat of vaporization | (J.kg ⁻¹) |
| ΔH_{total} | Total heat of desorption | (J.kg ⁻¹) |
| $\Delta H_{wetting}$ | Heat of wetting | (J.kg ⁻¹) |
| φ | Heat flux density | (W.m ⁻²) |
| ω | Rotation speed | (rpm) |

Subscripts

| | |
|-----|------------|
| DM | Dry matter |
| eff | Effective |
| i | Position |
| L | left |
| R | right |
| s | Sludge |
| v | Vapor |
| w | Water |

REFERENCES

- [1] Arlabosse, P., Chavez S., 2004, Influence of the phosphoric acid addition on the drying kinetic of dredged sediment, Proceeding of the International Drying Symposium, Sao Paulo (Brasil).
- [2] Ferrasse, J.H., Arlabosse, P., and Lecomte, D., 2002, Heat, Momentum and Mass Transfer Measurements in Indirect Agitated Sludge Dryer, *Drying Technology*, 20(4&5), pp. 749-769.
- [3] Keey, R.B., 1978, *Introduction to Industrial Drying Operations*, Pergamon Press, Oxford

- [4] Reidel L., 1977, Calorimetric determination of the heat of hydration of foods., Chem. Mikrobiol. Lebensm, Vol. 5. (in German).
- [5] Siperstein F., Gorte R. J., Myers A. L., 1999, A new calorimeter for simultaneous measurement of loadings and heats of adsorption from gaseous mixtures, Langmuir, n°15, pp. 1570-1576.
- [6] Ruthven D. M., 1984, Principles of adsorption and adsorption processes, John Wiley & Sons, NY.
- [7] Nunes R.V., Rotsein E., 1991, Thermodynamics of the water-foodstuff equilibrium, Drying Technology, Vol. 9, pp. 113-137.
- [8] Ritzi, S.S.H., 1986, Thermodynamic properties of foods in dehydration, Engineering Properties of Foods, Rao, M.A. and Ritzi S.S.H., Eds., Marcel Dekker, Inc., NY
- [9] Ferrasse, J.H., Lecomte, D., 2004, Simultaneous heat-flow differential calorimetry and thermogravimetry for fast determination of sorption isotherms and heat of sorption in environmental or food engineering, Chemical Engineering Science, 59, n°6, pp. 1365-1376.
- [10] Fudym, O., Carrère Gée, C., Lecomte D. and Ladevie B., 2003, Drying kinetics and heat flux in thin-layer conductive drying, Int. Comm. Heat Mass Transfer, Vol. 30, n°3, pp. 333-347.
- [11] Herwijn, A.J.M., 1996, Fundamental aspects of sludge characterization, PhD Dissertation, Eindhoven Univ. Of Technol., The Netherlands
- [12] Chen G.W., Hung W.T., Chang I.L., Lee S.F. and Lee D.J., 1997, Continuous classification of moisture content in waste activated sludges, Journal of Environmental Engineering, 123, pp. 253-258
- [13] Laidler K.J. and Meiser J.H., 1982, Physical Chemistry, Benjamin Cummings Publishing Co., London.
- [14] Kemp, I.C., Fyhr, B.C., Laurent, S., Roques, M.A., Groenewold C.E., Tsotsas, E., Sereno, A.A., Bonazzi C.B., Bimbenet, J.J. and Kind M. (2001), Methods for processing experimental drying kinetics data, Drying Technology, (19), 1, pp. 15-34.
- [15] Chen, G., Yue, P.L., Mujumdar, A.S., 2002, Sludge dewatering and drying, Drying Technology, (20)4&5, pp. 883-916.
- [16] Yamahata, Y. and Izawa, H. (1984), Experimental study on application of paddle dryers for sludge cake drying, Proceedings of the 4th International Drying Symposium, IDS'84, Kyoto, pp. 719-724.

TABLES

Table 1 – Distance between the right (l_{iR}) or the left (l_{iL}) edges of the ring area and the position of the thermocouple.

| r_i (m) | l_{iR} (m) | l_{iL} (m) |
|-----------|--------------|--------------|
| 0.015 | 0.005 | 0.015 |
| 0.055 | 0.010 | 0.035 |
| 0.075 | 0.015 | 0.010 |
| 0.095 | 0.005 | 0.005 |

Table 2 – Characteristics of the two investigated sewage sludge

| Sludge | Process | $W_{initial}$ (kg /kg DM) | Volatile solid content (% of DM) | Carbon (% of DM) | Oxygen (% of DM) | Hydrogen (% of DM) | Nitrogen (% of DM) |
|--------|---------------------|------------------------------|-------------------------------------|---------------------|---------------------|-----------------------|-----------------------|
| A | Anaerobic digestion | 4.64 | 68.9 | 36.4 | 18.8 | 5.5 | 5.7 |
| B | Aeration | 3.54 | 86 | 46.7 | 22.1 | 6.9 | 7.3 |

Table 3 – Optimized parameters used to compute the change in the specific heat with the temperature

| Sludge | β | δ | Correlation coefficient |
|--------|---------|----------|-------------------------|
| A | 3.2 | 1077.2 | 0.9978 |
| B | 3.29 | 1434 | 0.9965 |

Table 4 – Transition moisture contents and evaporating flow rates per unit surface of the dryer for the three sludge consistency

| Sludge | W_{lumpy} (kg /kg DM) | W_{granular} (kg /kg DM) | $\frac{\dot{m}}{m}$ fluid | $\frac{\dot{m}}{m}$ lumpy | $\frac{\dot{m}}{m}$ granular |
|--------|-----------------------------------|--------------------------------------|------------------------------|------------------------------|---------------------------------|
| A | 2.75 | 0.27 | 29.7 | 10.5 | 7.8 |
| B | 2.99 | 0.32 | 12.4 | 11.5 | 13.8 |

FIGURES

Figure 1 – Detail of the heated wall of the dryer

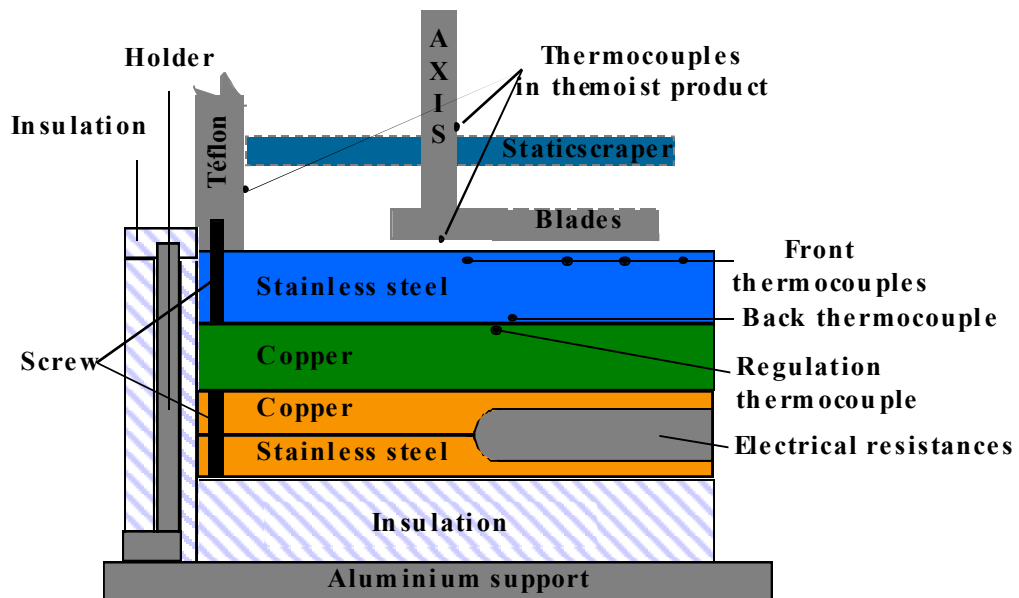


Figure 2 – Evolution of the torque required to maintain a constant rotation speed in the dryer (sludge A,

$T_{reg} = 180^{\circ}\text{C}$, $m_{ini} = 3.5 \text{ kg}$)

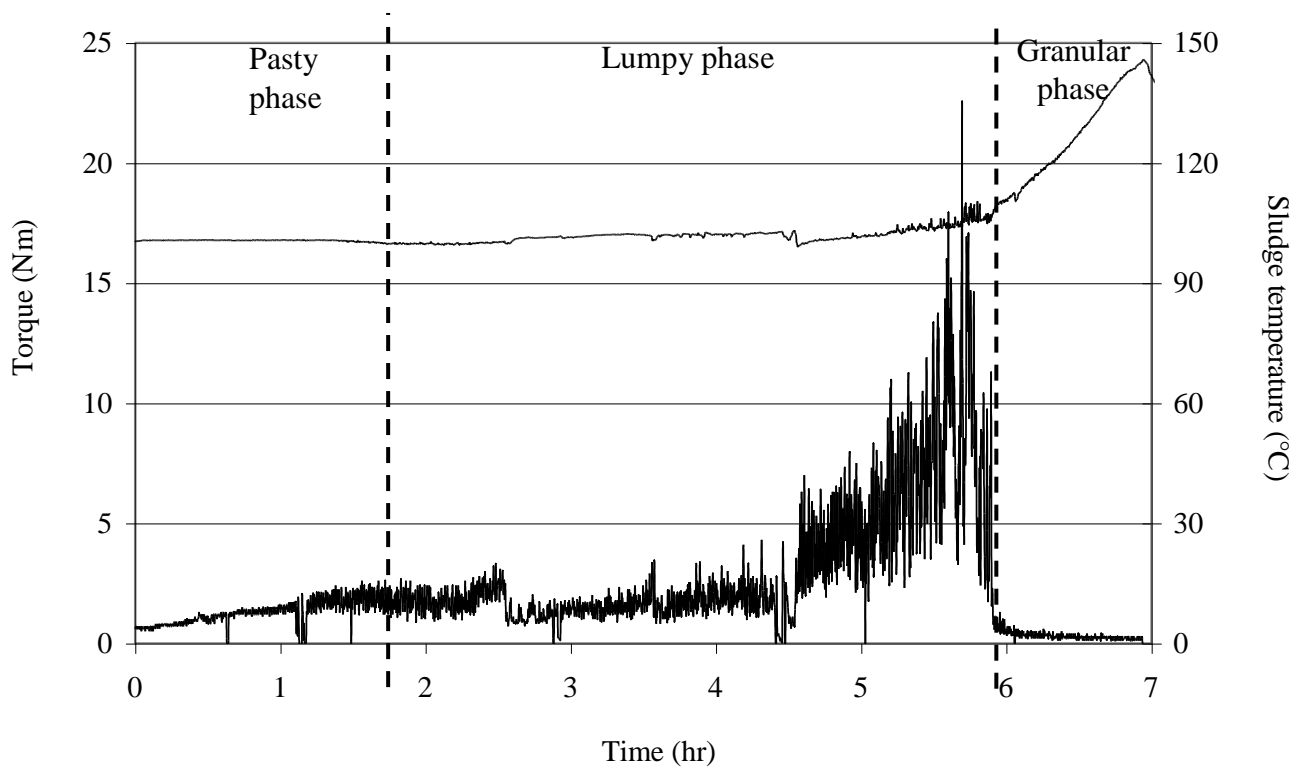


Figure 3 – Heat of wetting measured at 95°C (sludge A).

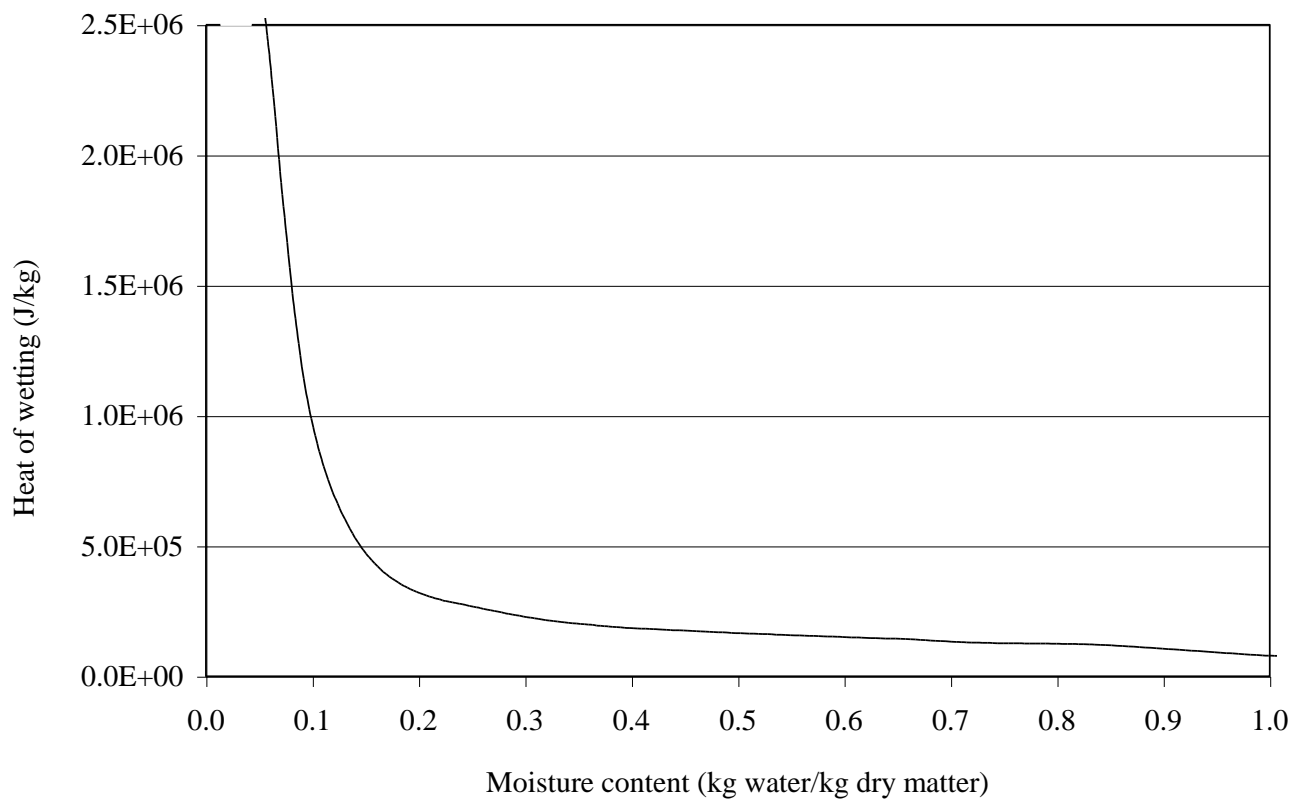


Figure 4 – Evolution of the wall heat flux density during the drying experiment (sludge A, $T_{reg} = 180^{\circ}\text{C}$, $m_{ini} = 3.5 \text{ kg}$)

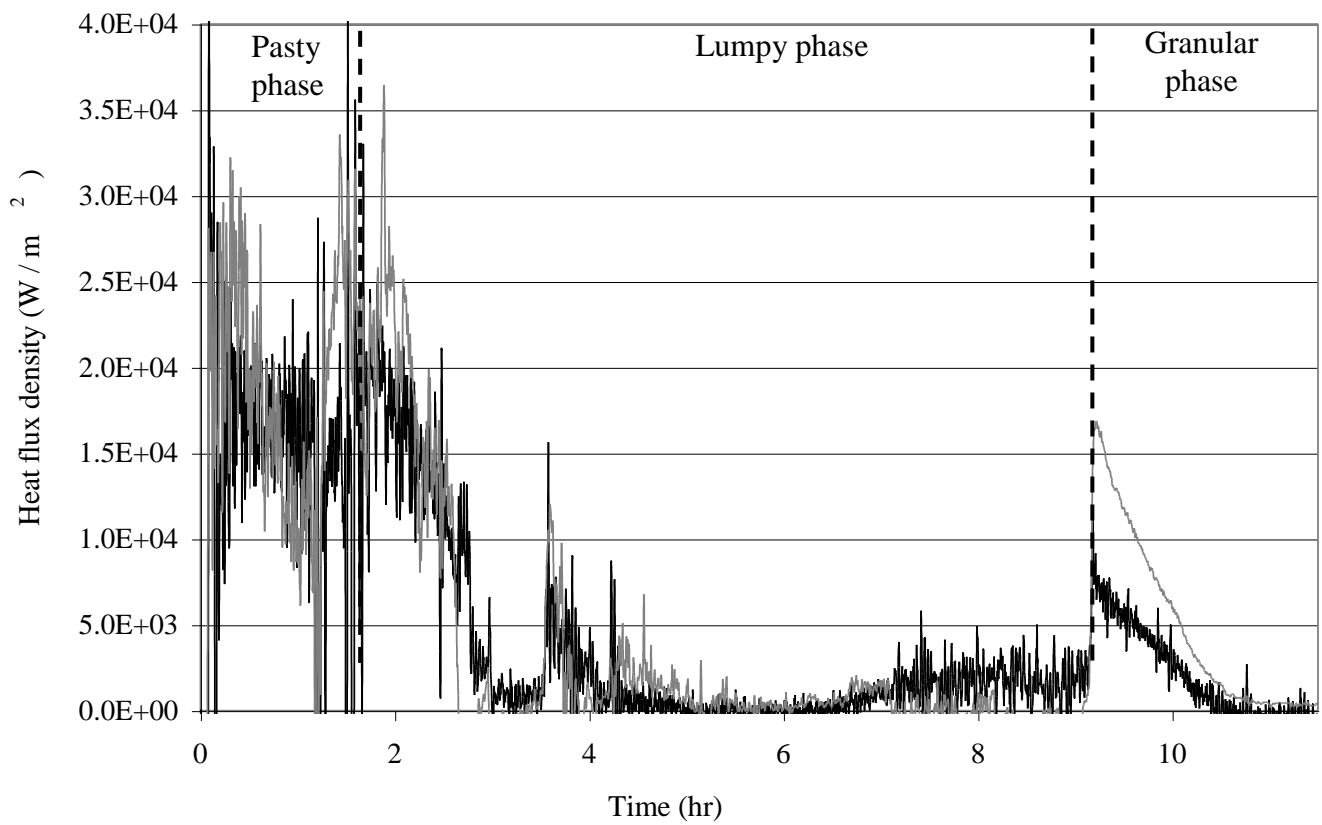


Figure 5 – Comparison between the measured and computed drying kinetics in the batch agitated dryer
(sludge A, $T_{reg} = 180^{\circ}\text{C}$, $m_{ini} = 3.5 \text{ kg}$)

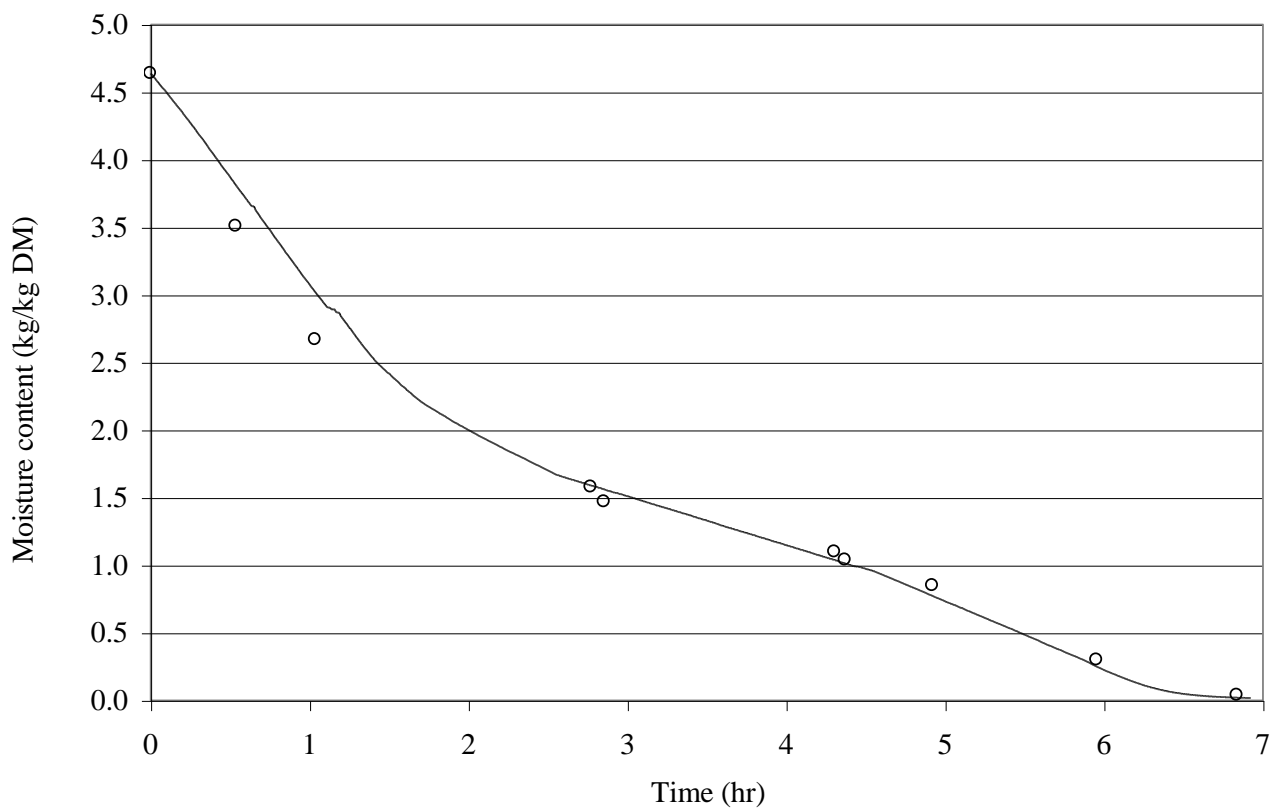


Figure 6 – Drying rate curve (sludge A, $T_{reg} = 180^{\circ}\text{C}$, $m_{ini} = 3.5 \text{ kg}$)

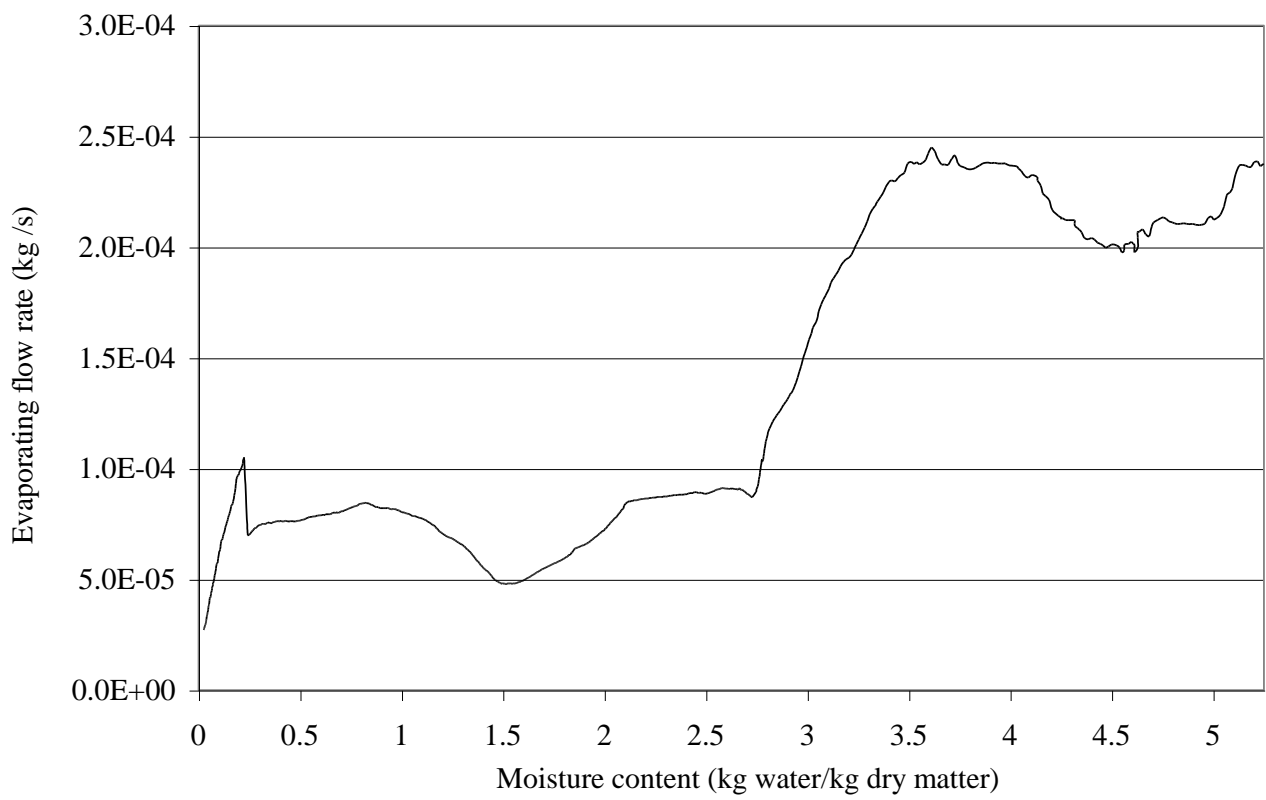


Figure 7 – Evolution of the computed (line) and measured (↔) moisture content along the dryer

